Author 1

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Tasmin		Hossain	member	thossai@ncsu.edu	yes

20

19

Affiliation for Author 1

Organization	Address	Country	URL or other info.
Department of Biological	3100 Faucette Dr, Campus	USA	
and Agricultural	Box 7625, Raleigh, NC		
Engineering, North	27695		
Carolina State University			

21

Author 2

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Daniela		Jones	Member, Professor	dsjones5@ncsu.edu	no

22

Affiliation for Author 2

Organization	Address	Country	URL or other info.
Department of Biological	3100 Faucette Dr, Campus	USA	
and Agricultural	Box 7625, Raleigh, NC		
Engineering, North	27695		
Carolina State University			

23

24

Author 3

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Damon		Hartley		damon.hartley@inl.g ov	no

Affiliation for Author 3

25

Organization	Address	Country	URL or other info.

Bioenergy Analysis,	2525 Fremont Ave, Idaho Falls,	USA	
Idaho National	ID 83415		
Laboratory			

Author 4

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Mike		Griffel		mike.griffel@inl.gov	no

27

Affiliation for Author 4

Organization	Address	Country	URL or other info.
Bioenergy Analysis, Idaho National Laboratory	2525 Fremont Ave, Idaho Falls, ID 83415	USA	

28

Author 5

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Yingqian		Lin		yingqian.lin@inl.gov	no

29

Affiliation for Author 5

Organization	Address	Country	URL or other info.
Bioenergy Analysis, Idaho National Laboratory	2525 Fremont Ave, Idaho Falls, ID 83415	USA	

30

Author 6

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Pralhad		Burli		pralhad.burli@inl.go v	no

31

	Affiliation for Au	thor 6	
Organization	Address	Country	URL or other info.

Bioenergy Analysis,	2525 Fremont Ave, Idaho Falls,	USA	
Idaho National	ID 83415		
Laboratory			

Author 7

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
David	N.	Thompson		david.thompson@inl .gov	no

33

Affiliation for Author 7

Organization	Address	Country	URL or other info.
Bioenergy Analysis, Idaho National Laboratory	2525 Fremont Ave, Idaho Falls, ID 83415	USA	

Author 8

34

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Matthew		Langholtz		langholtzmh@ornl.g ov	no

35

Affiliation for Author 8

Organization	Address	Country	URL or other info.
Environmental	P.O. Box 2008, Oak Ridge, TN	USA	
Sciences Division, Oak	37831		
Ridge National			
Laboratory			

36

Author 9

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Maggie		Davis		davismr@ornl.gov	no

Affiliation for Author 9

Organization	Address	Country	URL or other info.
Environmental	P.O. Box 2008, Oak Ridge, TN	USA	
Sciences Division, Oak	37831		
Ridge National			
Laboratory			

Author 10

First Name or initial	Middle Name or initial	Surname	Role (ASABE member, professor, etc.)	E-mail (and phone for contact author)	Contact author? yes or no
Craig		Brandt		brandtcc@ornl.gov	no

Affiliation for Author 10

Organization	Address	Country	URL or other info.
Environmental Sciences Division, Oak Ridge National Laboratory	P.O. Box 2008, Oak Ridge, TN 37831	USA	

2 3

THE NTH-PLANT SCENARIO FOR BLENDED FEEDSTOCK CONVERSION AND PREPROCESSING NATIONWIDE: BIOREFINERIES AND DEPOTS

4 Highlights

- Nationwide facility database to meet target cost, quality and quantity for biofuels.
- In 2022, 42.8M dt of corn stover and switchgrass could be accessible nationwide
- An \$8/dt reduction in delivery cost could reduce total accessible biomass by 67%.
- KS, NE, SD and TX were identified as potential states with a strong biofuel economy
- CO, AL, GA, MN, MS and SC could greatly benefit from a nationwide depot network.

10 **ABSTRACT.** The sustainability of the biofuel industry depends on the development of a mature 11 conversion technology on a national level that can take advantage of the economies of scale: the nth-12 plant. Defining the future location and supply logistics of conversion plants is imperative to transform the nation's renewable biomass resources into cost-competitive, high-performance feedstock for 13 production of biofuels and bioproducts. With US restrictions on production levels of conventional 14 biofuels from edible resources, the nation needs to plan for the widespread accessibility and 15 16 development of cellulosic biofuel. Conventional feedstock supply systems will be unable to handle cellulosic biomass nationwide, making it essential to expand the industry with an advanced feedstock 17 18 supply system incorporating a distributed network of preprocessing depots and biorefineries. Current 19 studies are mostly limited to designing supply systems for specific regions of the country. We developed 20 a national database with potential locations for depots and biorefineries to meet the nation's target 21 demand of cellulosic biofuel. Blended feedstock are considered in a Mixed Integer Linear Programming 22 model to deliver on-spec biomass with a desired quantity and quality at the biorefinery. A total delivered 23 feedstock cost that is less than \$79.07/dt (2016\$) is evaluated for years 2022, 2030, and 2040. In 2022, 24 124 depots and 59 biorefineries could be supplied with 42.8 million dt of corn stover and switchgrass. 25 In 2030 and 2040, the total accessible biomass could increase to 215% and 393% respectively when 26 compared to 2022. However, an *\$8/dt* reduction in targeted delivery cost reduces the total accessible 27 biomass by 67%. Kansas, Nebraska, South Dakota and Texas are potential states with a strong biofuel 28 economy as they had six or more biorefineries located in all scenarios. Colorado, Alabama, Georgia,

- 29 Minnesota, Mississippi and South Carolina would greatly benefit from a depot network as these could
- 30 only deliver to a biorefinery in a nearby state. To elaborate the impact of a nationwide consideration,
- 31 the findings were compared with existing literature for different US regions.
- 32 Keywords. Corn stover, Switchgrass, Biofuel, Feedstock quality, Biomass supply chain, Mixed-integer
- 33 *linear programming*

INTRODUCTION 34

Feasibility studies of agricultural residue conversion to biofuels, bioproducts, and/or biopower are 35 36 on the rise given biomass' potential to become the major source of US renewable energy (Langholtz et al., 2016). The goal is to mitigate the negative impact of climate change and provide energy security. 37 38 Currently, the most widely produced biofuel is conventional ethanol (derived from corn starch) which 39 is an effective substitute for fossil fuel in the transportation industry. The US is one of the largest fuel 40 ethanol producers in the world with 200 plants that total a national name plate production capacity of 41 over 16.9 billion gallons (US EIA, 2019), 42% of the global biofuel production share (IEA, 2019). To 42 restrict competition of food resources and pressure on arable lands, US has limited the production of conventional biofuels to 15 billion gallons per year (BGY) and set a target of 21 BGY of non-edible 43 44 feedstock to boost the total renewable fuel production by 2022, from which at least 16 BGY should be 45 from cellulosic biofuels (US EPA, 2020). Unlike food-based biomass resources, cellulosic biomass are 46 non-edible resources including energy crops, municipal solid waste, and agricultural or forest residues 47 (Kim and Dale, 2015). Due to widespread availability and low-cost raw material, cellulosic biomass is 48 a promising alternative for starch-based biomass. But, the biofuel production cost is unclear due to the 49 complex preprocessing operations, transportation and storage conditions (Limayem & Ricke, 2012). 50 Since the cellulosic biofuel production in the US was unable to meet the predictions for year to date, 51 EPA reduced the volume required to comply with RFS2 (US EPA, 2020). EPA had previously demanded

- 10.5 billion gallons of cellulosic biofuel production for year 2020, but had to reduce their targets to 590 52
- 53 million gallons (Bracmort, 2018). This production shortage could be overcome with an efficient supply ASABE Journal Template July 2020

54 chain. Currently, we rely on a conventional/centralized supply system where feedstock is harvested, 55 baled and stored close to their provenance and transferred directly to biorefineries. Given the inherent 56 non-flowable and bulky characteristics of agricultural residues, this system is not efficient in handling cellulosic resources. Several studies have shown that, this system fails to handle supply regions with 57 lower yield and larger supply area (Lamers et al., 2015a; Jacobson et al., 2014; Hess et al., 2009a). 58 59 Logistic complexities stems partly from their dispersed geographic location, and quality variability. 60 Therefore, the feedstock logistics for cellulosic biofuel constitutes 35-50% of the production cost, which 61 constraints the near-term development of a consistent market (Foust et al., 2007).

62 An advanced feedstock supply system that ensures the delivery of on-spec biomass at the gate of 63 biorefinery would reduce production costs and accelerate the national biofuel industry (Hess et al., 64 2009b). The idea is to move biomass-preprocessing operations from the biorefinery closer to the farmgate and into preprocessing depots. These smaller facilities, when compared to biorefineries, could 65 66 be built in the lower yielding regions not accessible by conventional biorefineries (Argo et al., 2013), 67 depots will help increase the biomass supply region. Depots would receive biomass with heterogeneous characteristics and provenance from nearby regions for drying, grinding, and densification to a uniform 68 69 format feedstock (Hess et al., 2009b). Shipments to biorefineries would be based on a biomass 70 blend/ratio with specified qualities including ash, moisture and carbohydrate content. Because the focus 71 has been to design a cellulosic biofuel supply chain that maximizes quantities delivered at a biorefinery, 72 very few studies have used the concept of biomass blending for on-spec deliveries (Campbell et al., 73 2013; Shi et al., 2013; Roni et al., 2018; Eksioğlu et al., 2020; Narani et al., 2019). Blending costs 74 depend on quality targets for different conversion pathways. Feedstock blend that meets target ash and 75 carbohydrate content costs 12.12% higher than only meeting the latter (Roni et al., 2018).

Finding the location and size of the depots and biorefineries alongside with identifying the optimum feedstock blend and logistics cost, can ensure a long-term financial stability of the cellulosic biofuel production. A cost-competitive and efficient system design requires the integration of the

79 interdependencies and complexities of all the different supply chain stages. Some studies in the 80 literature considered a single feedstock (Kim et al., 2016; Lin et al., 2016) while others considered 81 multiple feedstock types (Zhu et al., 2011; Marvin et al., 2012). Almost all of the studies have considered a regional supply area. Gonzales et al. (2017) developed a GIS-based heuristic to identify 82 83 depots and biorefineries nationwide to locate stranded and accessible herbaceous biomass. The study 84 did not consider on-spec delivery within a target cost. Eksioğlu et al. (2009) identified the location, size 85 and number of biorefineries as well as average travel distance and transportation costs to produce 86 cellulosic ethanol from corn stover in Mississippi. Bai et al. (2011) proposed Lagrangian Relaxation 87 (LR) based heuristics to predict biorefinery locations in Illinois for optimum biorefinery investment, 88 feedstock and transportation cost. Marvin et al. (2012) developed a mixed-integer linear programming 89 (MILP) model which can handle five different types of agricultural residues to determine the optimal 90 location and size of biorefineries for a nine-state region in Midwestern US. Ng et al. (2017) developed 91 an MILP model with multi-year horizon to minimize total annual cost determining the optimal number, 92 capacity and location of depots and biorefineries, the production inventory and shipment profiles. Corn 93 stover and switchgrass was considered to use the model in Southern Wisconsin.

94 Feedstock cost include, (1) grower payment, (2) logistics cost, and (3) quality costs. Most of the 95 studies found in literature optimized logistics cost while maximizing supply. Delivering the optimal 96 feedstock blend to the biorefinery considering both quality and quantity of feedstock, is still in its 97 infancy in terms of research. Roni et al. (2019) developed an MILP model to optimize feedstock 98 sourcing decisions and depot locations while considering a least-cost blend formulation for multiple 99 feedstock (agricultural residues, energy and municipal solid waste). The quality biomass parameters 100 considered by Roni et al. (2019) were carbohydrate, ash and moisture content to identify the optimum 101 feedstock blend to feed biorefinery in Kansas. The authors only considered the supply chain for a single 102 biorefinery while identifying the depot locations. Since cellulosic biomass is costly to handle and 103 transport, higher production cost puts another limitation to the advancement of this industry alongside

with the quality constraints. DOE goal is to achieve a near-term \$3/GGE by 2022 or a long-term goal
of \$2.5/GGE by 2030, where feedstock handling and delivery costs are \$71.26/dt and \$79.07/dt
respectively at the biorefinery gate (Davis et al., 2013).

107 The authors identified a knowledge gap in the literature that no other studies consider a nationwide 108 delivery of on-spec biomass to depots and biorefineries while meeting a target minimum fuel-selling 109 price of \$3/GGE by 2022 and \$2.5/GGE by 2030. This study aims to fill in that research gap by 110 optimizing both the logistics cost and quality costs while handling the complexities of nationwide 111 delivery under a target biofuel price. The novelty in this study is that we provide an economically and 112 technically viable industry path to the development of a national biofuel industry by answering some 113 of the key questions: i) How much biomass can be delivered nationwide under the quality and cost 114 target? ii) What are the logistics cost required for delivery? iii) What are the optimum locations and 115 capacities of depots and biorefineries nationwide? iv) What are the possible scenarios for various states 116 in a depot-based system? To answer these, we developed a modified version of the least-cost 117 formulation model (Roni et al., 2020). Contributions from this study: (1) Validation that a larger supply 118 radius and a higher quantity of biomass can be accessed using a distributed system of depots to meet 119 competitive biofuel prices. (2) Exemplary scenarios with a national mature conversion technology that 120 takes advantage of economies of scale, the nth-plant scenario. (3) Contribution to the literature with a 121 public nationwide database of field-depot and depot-biorefinery location and allocation considering 122 multiple scenarios to meet DOE near- and long-term cost targets.

123 **Methods**

124 MODEL APPROACH

The mixed-integer linear program (MILP) model was developed using the OPTMODEL procedure in SAS Institute Inc. 9.4M4 and the brand and cut algorithm was used to solve the model. The MILP analyzes different biomass feedstock quantities available at various farmgate prices as well as routes from fields to candidate depot sites where it goes through pretreatment and blending with other types 129 of biomass. Routes from depots to biorefineries are also analyzed to ship a blend of different feedstock 130 types. Figure 1(a) represents the decision network used to formulate the distributed depot system and 131 includes different farmgate price levels, feedstock types, field locations, depot locations, and biorefinery locations. The MILP solves for the maximum amount of biomass feedstock shipped nationwide while 132 133 meeting a set of biomass characteristics or quality specifications, cost and capacity constraints. In the 134 solution, all biorefineries are co-located with a depot to minimize the transportation cost. Depots that 135 are co-located with biorefineries are in high yielding regions and have a capacity as large as the 136 biorefinery. Smaller depots help collect biomass from lower yielding regions and ship the preprocessed 137 feedstock to biorefineries in higher yielding regions. Model inputs included: the resource quantities 138 presented in the BT16 by Oak Ridge National Laboratory (Langholtz et. al, 2016), the targeted delivery 139 feedstock cost to the reactor throat presented by the National Renewable Energy Laboratory for 140 biochemical conversion (Davis et al., 2013), and logistics costs presented by Roni et al., (2018).

141 MODEL INPUTS

142 Available biomass

The base-case scenario county-level feedstock values reported in the BT16 for years 2022, 2030 and 143 2040 at farmgate prices between \$30-50 (table 1) were inputs to the model (Langholtz et al., 2016). 144 145 Note that the BT16 supply curves are developed by multiple iterations of different price runs and should 146 be interpreted as either a total of available feedstock x at \$30, \$40 or \$50, and not a cumulative total at 147 all farmgate prices. For example, in 2022, there is 29.5 Mdt (million dry tons) of corn stover at \$40/dt 148 or 89.9 Mdt of corn stover at \$50/dt. We assumed that a biorefinery will accept a feedstock blend of switchgrass and corn stover. The blend will contribute towards achieving quality specifications at the 149 150 biorefinery. Delivering on-spec biomass, includes feedstock with ash content less than or equal to 5% 151 (dry basis), moisture content equal to 20% and carbohydrate content greater than or equal to 59% 152 (Davis et al., 2013). A key approach in obtaining the quality requirements of a feedstock is to modify 153 the harvest operation (Langholtz et al., 2019). Two-pass corn stover has around 4% less ash content and higher carbohydrate content than three-pass (Shinners et al., 2012). However, the per acre yield of two-154

- 155 pass is lower compared to three-pass. The decrease in yield is compensated using a corn stover factor
- 156 which assumes that two-pass harvest yield is 49% less than three-pass (Langholtz et. al, 2016). Both
- 157 corn stover harvesting operations are choices for the model.

Year	Feedstock	Available biomass (million dry tons) based on farmgate prices (\$/dry tons)		
		\$30	\$40	\$50
2022	CS	0	29.5	89.9
	SW	0	0.12	13.2
2030	CS	16.7	36.1	116
	SW	0	4.05	59.1
2040	CS	32.7	44.5	144
	SW	0	27	142

158 Table 1. Nationwide supply curves for corn stover (CS) and switchgrass (SW)

159 Field locations

US counties were considered fields in our model. Given that cropland is not equally distributed through counties, the spatial location of cropland in the 2018 CDL (classified as corn, cotton, rice, sorghum, soybeans, barley, durum wheat, spring wheat, winter wheat, oats, and fallow/idle) was used to geo-reference available biomass at each county as an alternative to using county centroids and was best illustrated in Ashley, AR and Washakie, WY Counties (fig. 1(b)). On average, the difference in centroids was 0.074° (8.2 km) with the highest change been 0.8° (89 km) in San Miguel County, NM.



166

- Figure 1. (a) Schematic representation of the decision network analyzed where CS2P is two-pass corn stover, CS3P is three-pass corn stover, and SW is switchgrass. (b) Cropland centroids vs county centroids.
- 169 Logistic costs

Table 2 presents the logistics costs used in this study based on Roni et al. (2018). The fixed transportation cost for bales is almost four times higher than the cost for pellets. Storage for bales is almost 11 times greater than that of pellets. The ash dockage and moisture dockage cost were considered when the feedstock failed to meet the ash and moisture specifications.

174 Table 2. Costs for Advanced Supply Chain (2016\$)

Cast Dansintian	Ess data da Essura d	T ti		Feedstoo	ck
Cost Description	Feedstock Format	Location	CS3P	CS2P	SW
Farmgate Price	Bale	Field	\$30-	-50 ^[a]	\$30-50 ^[a]
Storage	Bale	Field	\$3.97	\$4.10	\$3.02
Storage, Handling and Queuing	Bale to pellets	Depot	\$2	.09	\$2.22
Storage, Handling and Queuing	Pellets	Biorefinery	\$0	.34	\$0.65
Processing Cost	Bale to pellets	Depot	\$19	9.47	\$18.77
Ash Dockage	Pellets	Biorefinery	\$2.71	\$0.98	\$0.53
Moisture Dockage	Pellets	Biorefinery	\$0.03	\$0.03	\$0.03
Transportation Fixed Cost or Field-side Handling and Queuing	Bale	Field to Depot		\$3.42	
Transportation Variable Cost ^[b]	Bale	Field to Depot		\$0.114	1
Transportation Fixed Cost	Pellets	Depot to Biorefinery	\$0.	829	\$0.792
Transportation Variable Cost ^[b]	Pellets	Depot to Biorefinery	\$0.	082	\$0.081

175 [a] 2014\$, [b] *\$/mile. CS3P= Corn stover 3-pass, CS2P= Corn stover 2-pass, and SW= Switchgrass.

176 Candidate depot and biorefinery locations

Given the computational complexities of an uncapacitated facility location problem with a nationwide scope (2,082 possible locations for depots and biorefineries); we reduced the problem size to solve for optimality and used a two-step process. To find a subset of candidate locations, we solved to maximize corn stover (three-pass only) and switchgrass delivered at \$79.07 /dt to depots using the biomass supply curve for year 2040 in the BT16 and relaxed the quality constraints. This initial solution found a total of 98.6 Mdt delivered to 247 depots, which were used as candidate locations for depots and/or biorefineries in the MILP model presented in this paper.

184 MODEL FORMULATION

The MILP model presented in this paper identifies the optimal location and size of an undetermined number of biorefineries and depots to maximize total feedstock delivered to biorefineries at less than or equal to a specific target price (eq. 1). We analyzed two target prices: \$79.07 and \$71.26 per dt (\$2016) based on the short- and long-term goals presented by a DOE techno-economic analysis (Davis et al., 2013). Table 3 presents the data sets, parameters, and decision variables in our MILP formulation.

190

191

$\max \sum_{j \in J} \sum_{k \in K} \sum_{f \in F} x_{jkf}$	(1)
JCJ KCK JCI	

Data s	ets		
F	Set of feedstock types	α_f	Set of ash content per ton for feedstock f
Р	Set of feedstock prices	μ_f	Set of moisture content per ton for feedstock f
ŗ	Set of field locations	β_f	Set of carbohydrate content per ton for feedstock f
r	Set of potential depot locations	a_{ifp}	Set of available supply for field i of feedstock type f at price p

Table 3. Data sets, parameters, and decision variables

K	Set of potential biorefinery locations		Set of minimum supply for field <i>i</i> of feedstock type <i>f</i>	
d _{ii}	Set of distances between location i and location j		Set of distances between location j to location k	
VC _{ijkfp}	Set of total variable cost from field <i>i</i> to depot <i>j</i> : farmgate price (gr), VC_{ijkfp} storage (sb, sp), transportation (trb, trf), handling and queuing (qh), preprocessing costs (pr), ash dockage (ad) and moisture dockage (md)			
Paramet	ers			
Т	Cost target at delivery	Η	Target carbohydrate content at biorefinery	
U	Required depot utilization factor (90%)		Demand of a biorefinery	
M	Minimum moisture content at biorefinery	S	Constant multiplier for depot capacity	
Α	Maximum ash content at biorefinery			
Decisior	n Variables			
C_j	Factor for depot capacity at location <i>j</i> (integer)	Z_{ifp}	1 if feedstock <i>f</i> is purchased at price <i>p</i> from location <i>i</i> ; 0 otherwise (binary)	
X_{ifp}	Amount of feedstock f purchased at price p from location i (integer)		1 if depot is built in location <i>j</i> ; 0 otherwise (binary)	
X_{ijf}	f_{ijf} Amount of feedstock f shipped from location i to location j (integer)		1 if biorefinery is built in location <i>k</i> ; 0 otherwise (binary)	
X_{jkf}	Amount of feedstock f shipped from location j to location k (integer)			

193 Demand at each biorefinery was constant at 725,000 dt/year (D). Depot capacities were determined 194 by the model using the product of a constant multiplier 25,000 (S) and an integer decision variable (C_i) . 195 Depot construction costs presented by Roni et al. (2019) fitted a linear equation with an adjusted R-196 square of 0.998. Equation 2 represents depot fixed costs (FC). Variable costs (VC) to deliver biomass 197 included farmgate price, storage, handling, transportation and preprocessing costs (eq. 3). When needed, 198 a cost to reduce ash or increase moisture was incurred at the biorefinery to meet quality specifications. 199 Constraints in table 4: (1) ensures that each feedstock is purchased only at a single price from each field 200 location. (2) Puts a maximum limit to the amount of feedstock purchased from a field location so that it does not exceed the total amount available at that field. (3) Ensures that the total amount of corn 201 202 stover harvested from a location using three-pass and two-pass is not more than the available corn stover 203 in that field. (4) Decides on the capacity of the depot depending on the total supply to that depot. (5) Is 204 the flow balance between field and depot. (6) Sets a minimum utilization to the depot capacity. (7) Is 205 the flow balance between depot and biorefinery. (8) Ensures that the total supply to a biorefinery meets 206 the required demand. (9) Requires that the total carbohydrate content of all the different feedstocks 207 supplied to a biorefinery meet the minimum carbohydrate requirement. The cost target is bounded using 208 constraint (10) combining the total fixed as well as variable costs. The constraints in (11) ensures non-209 negativity of the integer decision variables. Constraints in (12) are for binary decision variables.

210
$$FC = \sum_{j \in J} (132,717 * L_j + 2.297 * (S * C_j))$$
(2)

211
$$VC_{ijkfp} = \sum_{i \in I} \sum_{f \in F} \sum_{p \in P} (0.997 * gr_p * X_{ifp}) + \sum_{i \in I} \sum_{f \in F} \sum_{j \in J} (sb_f + qh_f + pr_f + trb_{ijf} + sp_f) * X_{ijf} + \sum_{j \in J} \sum_{k \in K} \sum_{f \in F} (trp_{jkf} + (\alpha_f - A) * ad_f + (M - \mu_f) * md_f) * X_{jkf}$$
(3)

No.	Constraint Name	Mathematical Formulation
1	Feedstock purchase	$\sum_{n \in \mathbb{D}} Z_{ifp} \leq \begin{cases} 0 \text{ if } m_{if} = 0\\ 1 \text{ otherwise} \end{cases} ; \forall i \text{ in } I, f \text{ in } F$
2	Maximum supply	$X_{ifp} \leq a_{ifp} * Z_{ifp} \qquad ; \forall i in I, f in F, p in P$
3	Three pass & Two pass	$X_{i,f=CS3P,p} + \left(X_{i,f=CS2P,p} / CS Factor\right) \le a_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; I, f \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; i \; in \; F, p \; in \; X_{i,f=CS3P,p} \; ; \; \forall \; in \; F, p \; in \; X_{i,f=CS3P,p}$
4	Depot Capacity	$\sum_{i \in I} \sum_{f \in F} X_{ijf} \le S * C_j ; \forall \ j \ in \ J$
5	Flow balance for field-depot	$\sum_{p \in P} X_{ifp} = \sum_{j \in J} X_{ijf} if \ dij < 80 \ ; \ \forall \ i \ in \ I, f \ in \ F$
6	Depot Utilization	$\sum_{i \in I} \sum_{f \in F} X_{ijf} \ge U * S * C_j if \ d_{ij} < 80 ; \forall \ j \ in \ J$
7	Flow balance for depot-biorefinery	$\sum_{i \in I} X_{ijf} = \sum_{k \in K} X_{jkf} \text{ if } djk < 400; \forall j \text{ in } J, f \text{ in } F$
8	Biorefinery Demand	$\sum_{i \in I} \sum_{f \in F} X_{jkf} = D * L_k \qquad ; \forall k \text{ in } K$
9	Carbohydrate quality constraint	$\sum_{j\in J}\sum_{f\in F} X_{jkf}*\beta_f \ge H*\sum_{j\in J}\sum_{f\in F} X_{jkf} \qquad ; \forall k \text{ in } K$
10	Cost target	$FC_j + VC_{ijkfp} \le T * X_{jkf}$
11	Integer constraints	$ \begin{array}{ll} X_{ifp} > 0, \forall \ i \in I, \ f \in F, p \in P; \\ X_{jkf} > 0, \forall \ j \in J, \ k \in K, \ f \in F; \end{array} \begin{array}{ll} X_{ijf} > 0, \forall \ i \in I, \ j \in J, \ f \in F \\ C_j > 0, \forall \ j \in J \end{array} $
12	Binary constraints	$ \begin{array}{ll} Z_{ifp} \in \{0,1\}, & \forall \ i \in I, \ f \in F, \ p \in P \\ L_j & \in \{0,1\}, & \forall \ j \in J \\ L_k & \in \{0,1\}, & \forall \ k \in K \end{array} $

213 **Results**

214 SCENARIOS

215 Four different scenario runs were performed considering the year and cost target, namely (S1) 2022 216 at \$79.07/dt, (S2) 2030 at \$79.07/dt, (S3) 2040 at \$79.07/dt and (S4) 2030 at \$71.26/dt. Even after 217 decreasing the set of depot and biorefinery candidates, the problem had around 43,000 variables, 5,500 218 constraints and 16,000 constraint coefficients. We ran each scenario for 3 hours and obtained an error 219 gap between 12-13%. The results for the different years and targeted prices analyzed in this study are 220 presented in table 5. When targets for delivery to the reactor throat are at \$79.07/dt, the total viable 221 biomass collected has above a two-fold increase (215%) from 2022 to 2030 and almost a four-fold 222 increase (393%) from 2022 to 2040. The increase in total collected biomass could be explained by the

increase in biomass availability and inherent higher geographical concentration within regions, making it cost efficient to collect more biomass within the same cost target. While we see a significant increase in potential biomass delivered to biorefineries with respect to time, DOE has lower long-term cost targets for 2030 (\$71.26/dt). Based on our analysis, a lower delivering cost target would decrease the total available biomass in 2030 by 68% and 69% when comparing years 2030 and 2022 respectively.

228	Table 5. Analyzed scenarios

Saanaria	Foodstools	Million dry tons / year			ır	- Number of Facilities	Summary Statistics for	
Scenario	recusiock	\$30	\$40	\$50	Total	- Number of Facilities	Biorefinery costs (\$)	
S1: 2022 \$79.07/dt	$SW^{[a]}$	0	0.01	5.31	5.32	124 Daw sta	Min: \$71.36 Max: \$87.91 Standard dev.: 3.92	
	CS2P ^[b]	0	7.83	17.6	25.5	59 Biorefineries 42.8 Mdt Collected		
	CS3P ^[c]	0	9.14	2.85	12.0		Standard error: 0.51	
	SW ^[a]	0	3	35.4	38.4	204 Depots 127 Biorefineries 92.1 Mdt Collected	Min: \$63.61 Max: \$87.76 Standard dev.: 5.31 Standard error: 0.47	
S2: 2030 \$79.07/dt	CS2P ^[b]	2.16	9.21	21.8	33.2			
	CS3P ^[c]	10.3	4.18	6	20.5			
	SW ^[a]	0	17.8	60.6	78.4	304 Depots 231 Biorefineries	Min: \$63.64 Max: \$101.72 Standard dev.: 6.13 Standard error: 0.403	
S3: 2040 \$79.07/dt	CS2P ^[b]	2.54	13.4	30.9	46.9			
	CS3P ^[c]	24.1	4.22	13.9	42.2	168 Mdt Collected		
	$SW^{[a]}$	0	2.11	4.68	6.79	80 Depots 41 Biorefineries 29.7 Mdt Collected	Min: \$63.44 Max: \$80.59 Standard dev.: 4.62 Standard error: 0.722	
S4: 2030 \$71.26/dt	CS2P ^[b]	3.5	9.05	0.79	13.3			
	CS3P ^[c]	7.41	2.13	0.05	9.59			

229 ^[a] SW = Switchgrass, ^[b] CS2P = Corn stover two-pass, ^[c] CS3P = Corn stover three-pass.

230 SUMMARY STATISTICS

231 To further reduce our problem complexity, the cost constraint at the reactor throat was applied as an 232 average for a nationwide system. As a result, the solution located biorefineries with less than or equal to and greater than the target delivery cost. However, for an ideal scenario, all biorefineries would meet 233 234 the cost target. To observe the deviation from the cost target, the average cost for each individual 235 biorefinery was calculated. The highest deviation from the mean was observed in S4, with an average 236 cost of 95% of the biorefineries within +/- \$1.44 (=2*0.722) of the cost target \$71.26 /dt. This is due to 237 the limited supply of the scenario which makes it complex to build biorefineries at that lower cost target. 238 For all the other scenarios, the deviation was within +/- \$1. Figure 2(a) identifies minimum, maximum, 239 standard deviation, and standard error of the mean for all scenarios. 46, 39, 48 and 54% of all the 240 biorefineries were within the cost target for scenarios S1-S4 respectively.

241 **BIOMASS ACCESSIBILITY**

242 The BT16 data predicted that the availability of herbaceous biomass supply within the US would be enough to develop a sustainable biofuel economy. However, availability does not guarantee 243 244 accessibility of those biomass resources. Resources would be accessible only if they could be collected 245 and shipped to the gate of the biorefinery within a feasible cost. In figure 2(b) we identified the total percentage of stranded and accessible biomass based on the BT16 supply curve at the \$50 farmgate 246 247 price the total feedstock collected by the developed model in this study. A large portion of the feedstock 248 remained stranded or inaccessible when compared to the BT16 supply curve [fig. 2(b)]. Using costs for 249 the short- and long-term targets respectively, 45-60% and 20% of the available biomass was accessible 250 biomass with an advanced supply system. Hence, the goal of \$71.26/dt or \$2.5/GGE by 2030 might 251 only be achieved for 30 Mdt or 1.3 billion GGE (at 44.8 GGE/dt -Davis et al., 2013).

252 FEEDSTOCK RATIO

Figure 2(c) illustrates the estimated proportions of total feedstock type collected to maintain the onspec delivery. When the delivered target price is fixed, almost 50% of the total collected biomass is





model had to satisfy a lower cost target of \$71.26/dt. This resulted in the collection of biomass mostly
from the Corn Belt region. For the other two scenarios (S2 and S3), the input supply curve from BT16
at 2030 and 2040 was high enough to expand the selected regions by the model outside of the Corn Belt
and collect a higher percentage of switchgrass.

265 **DEPOT AND BIOREFINERY LOCATIONS**

Figure 3 is an illustration of our nationwide analysis for depot and biorefinery locations. The supply curve, represented in shades of green, was estimated using the average supply of corn stover and switchgrass at \$30, \$40 and \$50. Counties with an overlapping triangle and circle represent depots colocated with biorefineries. Moreover, the biorefineries that were within the cost target are mostly situated in the Corn Belt region and in part of Texas due to the higher biomass supply in those regions.



271

Figure 3. Depot and biorefinery locations in the US for four scenarios: (S1) 2022 @ \$79.07/dt, (S2) 2030 @ \$79.07/dt,
(S3) 2040 @ \$79.07/dt and (S4) 2030 @ \$71.26/dt.

274 **DEPOT AND BIOREFINERY CAPACITY**

275 The different capacities of depots built for all scenarios were also analyzed to estimate the scenario for

a conventional supply chain. Locations with a depot size of 725,000 dt could be identified as ideal for a conventional supply chain. For example, in S1, 13 biorefineries could be built with a conventional supply chain collecting 9.5 Mdt. Including depot locations allows for an increase of 42.8 Mdt collected biomass. The two most common depot sizes selected by the model are 725,000 and 25,000 dt/year. The biggest depot size reflects a co- location of a biorefinery and a depot minimizing delivery costs from depots to biorefineries. Interestingly, 114 depots of 625,000-700,000 dt/year were located across all the scenarios studied and only 89 depots of sizes 50,000-125,000.

283 STATEWIDE CAPACITY

Identifying the potential states with high number of depots and biorefineries could benefit the economies of scale of the supply chain system for those local regions (fig. 4).



286

Figure 4. Number of depots and biorefineries in each state for the four scenarios, (S1) 2022 at \$79.07/dt, (S2) 2030 at \$79.07/dt, (S3) 2040 at \$79.07/dt and (S4) 2030 at \$71.26/dt. The bubble size indicates the total amount of feedstock shipped to depots for each state. Each of the biorefineries have fixed demand of 725,000 dt/year.



291 more biorefineries located in all scenarios. NE was the only state with more than 10 biorefineries for

both, S1 and S4 suggesting that it can be a potential biofuel production base for both, the short-term and
long-term scenario. A few states had a very high number of biorefineries (>10): NE (S1, S2, S3, S4),
KS (S2, S3), TX (S2, S3), SD (S2, S3) and Ok (S2, S3). Some states had multiple depots but zero
biorefineries such as CO (S1, S4), AL (S2), GA (S4), MN (S4), MS (S4) and SC (S4). Those states
would need to ship the preprocessed biomass to a nearby out-of-state biorefinery. The number of such
cases increased with lower cost target introducing logistical complexities of longer haul.

298 **DISCUSSION**

The goal was to analyze the nationwide scenario for cellulosic biofuel production and determine the 299 300 feasibility of the EPA's target of 16 billion gallons by year 2022. Considering a biofuel yield of 44.8 301 GGE/dt (Davis et al. 2013), around 357 Mdt of feedstock needs to be delivered at the gate of the 302 biorefinery and a total of 493 biorefineries with 725,000 dt capacity each has to be built to meet EPA 303 goals. However, the results of the developed model indicated that only 42.8 Mdt of corn stover and 304 switchgrass could be delivered to a total of 59 biorefineries by year 2022 which is 12% of the total 305 cellulosic feedstock demand. The remaining 88% would come from other cellulosic resources including 306 miscanthus and wheat straw. But, given that corn stover and switchgrass comprise around 70% of the 307 total herbaceous supply (Langholtz et al., 2016), herbaceous biomass alone is not a feasible option. 308 Even when the supply curve of 2030 and 2040 from the BT16 was considered, the model predicted the 309 delivery of 26% and 47% of the EPA's cellulosic feedstock demand respectively.

A nationwide analysis helps identify an nth-plant scenario for biofuels, regardless of political boundaries, given that some states in the US may ship preprocessed biomass to the biorefinery of a nearby state. Optimizing part of the nation would have made the model computationally more efficient but it would introduce error in terms of boundary scenarios. The only previous work found in literature for a nationwide scenario was by Gonzales et al. (2017). However, Gonzales et al. (2017) did not consider on-spec delivery with quality nor specific constraints on the cost target. The study presented that 183.7 Mdt of herbaceous biomass could be collected out of the predicted 205 Mdt in year 2022 and 317 predicted to meet more than the targeted demand of EPA for year 2022. Our analysis suggested that the
318 EPA's target was highly over estimated if feedstock quality and biofuel price target were considered.

Roni et al. (2018) considered delivery to a single fixed biorefinery location in Seridan County of KS and solved to find depot locations and sizes for the least-cost feedstock blend. Four depots were identified in NE, KS and CO to supply a total of 725,600 dt to one biorefinery. In the same region, we identified 37 depots and 20 biorefineries in NE, KS and CO to supply a total of 14.5 Mdt [fig. 5(a)]. This difference may stem from solving for biorefineries and depots simultaneously and is reflected in a 20-fold increase of collected biomass when compared to Roni et al. (2018). In both cases, supply curves from the BT16 for 2022 were used.

326 Caffrey et al. (2015) used a simplified heuristic to analyze the biomass supply chain management in 327 North Carolina using Switchgrass and Sorghum with different harvest methods (e.g. forage and bales). 328 The storage location and biorefineries were determined using a conventional supply system. The authors 329 suggested that a biorefinery in the Coastal Plain region of NC would be beneficiary due to the higher 330 availability and productivity of agricultural feedstock in the region. The model results from the 331 presented study also suggested one biorefinery in NC close to the coastal region. Although, for year 332 2022, the available feedstock was not enough to meet the target cost of 79.07 \$/dt. Hence, the costal 333 biorefinery in NC was built only for the 2030 and 2040 scenarios [fig. 5(b)].



334

Figure 5. Magnifying on the location of depots and biorefineries in different states. Connecting lines indicate what fields are assigned to a depot (red circle) in the solution.

337 To overcome error gaps and model limitations, our future research will focus on running the model 338 on a super computer including all the field locations as potential depot and biorefinery candidates. The 339 model results were highly dependent on the cost parameters and the BT16 supply curve. A detailed 340 sensitivity analysis on the model parameters will also be included in our future work. Additionally, a 341 winding factor of 1.2 was included in the model for estimating the road distance. However, the existing 342 road network could be incorporated in the model to get real distances for an improved better estimate on the transportation and overall logistics cost. The authors plan is to modify the model presented to 343 344 analyze supply chains for additional and/or complementary biomass types such as miscanthus, short 345 rotation woody crops, and animal manure for conversion to fertilizers. Illustrating the versatility of the 346 developed model can be a valuable future aspect of this study.

347 **CONCLUSION**

To provide economic sustainability for cellulosic crop production, the location of cellulosic based 348 349 biomass depots and biorefineries have to be strategic throughout the US, creating sufficient cellulosic 350 biomass demand in the market and reducing the pressure on food production. Findings from this study 351 could be used to provide cost and profit analysis of cellulosic biofuel production to decision-makers 352 including supply managers, farmers and business investors and ensure a sustainable biofuel economy. 353 Both strong policy formulation and innovative conversion technology are required to meet EPA's 354 cellulosic biofuel production mandate. The results of this study pose a question whether the currently 355 set mandates are achievable and if they should be updated to a more realistic scenario.

356 ACKNOWLEDGEMENTS

Funded by DOE Energy Efficiency and Renewable Energy (EERE) Bioenergy Technology Office
under DOE Idaho Operations Office Contract DE-AC07-05ID14517 and USDA Hatch Project funds.
Views in this publication do not necessarily represent the views of the DOE or US Government. The
US Government retains and the publisher, by accepting the article for publication, acknowledges that

the US Government retains a nonexclusive, paid-up, irrevocable, worldwide license to publish or reproduce the published form of this work, or allow others to do so, for US Government purposes. We acknowledge help from SAS Inc. professionals for their valuable insights towards developing the MILP code: Lincoln Groves, Mark Hartmann, Tom Grant, Imre Pólik, and Rob Pratt. We are grateful to Mohammad S. Roni from INL for his excellent suggestions that helped in the analysis of this work.

366 References

- 367 Argo, A. M., Tan, E. C., Inman, D., Langholtz, M. H., Eaton, L. M., Jacobson, J. J., ... & Graham, R. L. (2013).
- 368 Investigation of biochemical biorefinery sizing and environmental sustainability impacts for conventional bale
- 369 system and advanced uniform biomass logistics designs. *Biofuels, Bioproducts and Biorefining*, 7(3), 282-302.
- 370 Bai, Y., Hwang, T., Kang, S., & Ouyang, Y. (2011). Biofuel refinery location and supply chain planning under
- 371 traffic congestion. Transportation Research Part B: Methodological, 45(1), 162-175.
- Balan, V., Bals, B., Chundawat, S. P., Marshall, D., & Dale, B. E. (2009). Lignocellulosic biomass pretreatment
 using AFEX. In *Biofuels* (pp. 61-77). Humana Press, Totowa, NJ.
- Bracmort, K. (2018). *The Renewable Fuel Standard (RFS): An Overview*. Washington, DC: Congressional
 Research Service.
- 376 Campbell, T. J., Teymouri, F., Bals, B., Glassbrook, J., Nielson, C. D., & Videto, J. (2013). A packed bed
- ammonia fiber expansion reactor system for pretreatment of agricultural residues at regional depots. *Biofuels*,
 4(1), 23-34.
- 379 Davis, R., Tao, L., Tan, E. C. D., Biddy, M. J., Beckham, G. T., Scarlata, C., ... & Knorr, D. (2013). Process design
- 380 and economics for the conversion of lignocellulosic biomass to hydrocarbons: dilute-acid and enzymatic
- deconstruction of biomass to sugars and biological conversion of sugars to hydrocarbons. No. NREL/TP-5100 60223.
- Ekşioğlu, S. D., Acharya, A., Leightley, L. E., & Arora, S. (2009). Analyzing the design and management of
 biomass-to-biorefinery supply chain. *Computers & Industrial Engineering*, *57*(4), 1342-1352.
- 385 Ekşioğlu, S. D., Gulcan, B., Roni, M., & Mason, S. (2020). A Stochastic Biomass Blending Problem in
- 386 Decentralized Supply Chains. *arXiv preprint arXiv:2006.06809*.

- 387 Foust, T. D., Wooley, R., Sheehan, J., Wallace, R., Ibsen, K., Dayton, D., ... & Hess, J. R. (2007). A national
- 388 laboratory market and technology assessment of the 30 x 30 scenario. *NREL, Golden, CO. 261p.*
- Gonzales, D. S., & Searcy, S. W. (2017). GIS-based allocation of herbaceous biomass in biorefineries and
 depots. Biomass and Bioenergy, 97, 1-10.
- 391 Hess JR, Kenney KL, Ovard LP, Searcy EM and Wright CT. (2009a). Commodity-scale production of an
- 392 infrastructure-compatible bulk solid from herbaceous lignocellulosic biomass. Contract No.: INL/EXT-09-
- 393 17527, Idaho National Laboratory, Idaho Falls, ID.
- 394 Hess JR, Wright CT, Kenney KL and Searcy EM. (2009b). Uniform-Format Solid Feedstock Supply System:
- 395 Commodity-Scale Production of an Infrastructure-Compatible Bulk Solid from Herbaceous Lignocellulosic
- Biomass, Report INL/EXT-09-15423, Idaho National Laboratory, Idaho Falls, ID.
- 397 IEA (2019). International Energy Agency. Biofuels production growth by country/region (2019, November 25).
- 398 Jacobson J, Cafferty K and Bonner I. (2014). A comparison of the conventional and blended feedstock design
- cases will be completed to demonstrate the potential of each design to meet the \$3/GGE BETO goal. IdahoNational Laboratory, Idaho Falls, ID, USA.
- 401 Kim, S., & Dale, B. E. (2015). Comparing alternative cellulosic biomass biorefining systems: Centralized versus
 402 distributed processing systems. *Biomass and Bioenergy*, *74*, 135-147.
- Kim, S., & Dale, B. E. (2016). A distributed cellulosic biorefinery system in the US Midwest based on corn
 stover. *Biofuels, Bioproducts and Biorefining*, *10*(6), 819-832.
- 405 Lamers, P., Roni, M. S., Tumuluru, J. S., Jacobson, J. J., Cafferty, K. G., Hansen, J. K., ... & Bals, B. (2015a).
- 406 Techno-economic analysis of decentralized biomass processing depots. *Bioresource technology*, *194*, 205-213.
- 407 Lamers, P., Tan, E. C., Searcy, E. M., Scarlata, C. J., Cafferty, K. G., & Jacobson, J. J. (2015b). Strategic supply
- 408 system design-a holistic evaluation of operational and production cost for a biorefinery supply chain. *Biofuels*,
- 409 *Bioproducts and Biorefining*, 9(6), 648-660.
- 410 Langholtz, M. H., Stokes, B. J., & Eaton, L. M. (2016). 2016 Billion-ton report: Advancing domestic resources
- 411 for a thriving bioeconomy, Volume 1: Economic availability of feedstock. Oak Ridge National Laboratory,
- 412 *Oak Ridge, Tennessee, managed by UT-Battelle, LLC for the US Department of Energy, 2016, 1-411.*
- 413 Langholtz, M., Eaton, L., Davis, M., Hartley, D., Brandt, C., & Hilliard, M. (2019). Cost and profit impacts of
- 414 modifying stover harvest operations to improve feedstock quality. Biofuels, Bioproducts and

- 415 Biorefining, 13(4), 1098-1105.
- 416 Limayem, A., & Ricke, S. C. (2012). Lignocellulosic biomass for bioethanol production: current perspectives,
- 417 potential issues and future prospects. *Progress in energy and combustion science*, *38*(4), 449-467.
- 418 Lin, T., Rodríguez, L. F., Davis, S., Khanna, M., Shastri, Y., Grift, T., ... & Ting, K. C. (2016). Biomass feedstock
- 419 preprocessing and long-distance transportation logistics. *Gcb Bioenergy*, 8(1), 160-170.
- 420 Marvin, W. A., Schmidt, L. D., Benjaafar, S., Tiffany, D. G., & Daoutidis, P. (2012). Economic optimization of a
- 421 lignocellulosic biomass-to-ethanol supply chain. *Chemical Engineering Science*, 67(1), 68-79.
- 422 Narani A, Konda NM, Chen C-S, Tachea F, Coffman P, Gardner J, et al. Simultaneous application of predictive
- 423 model and least cost formulation can substantially benefit biorefineries outside Corn Belt in United States: a
- 424 case study in Florida. Bioresour Technol 2019; 271:218–27.
- 425 Ng, R. T., & Maravelias, C. T. (2017). Design of biofuel supply chains with variable regional depot and
- 426 biorefinery locations. *Renewable Energy*, *100*, 90-102.
- Roni, M. S., Hartley, D. S., Griffel, M., Hu, H., Nguyen, Q. A., Cai, H., & Thompson, D. N. (2020). *Herbaceous feedstock 2018 state of technology report*. No. INL/EXT-18-51654-Rev000.
- Roni, M. S., Thompson, D. N., & Hartley, D. S. (2019). Distributed biomass supply chain cost optimization to
 evaluate multiple feedstocks for a biorefinery. Applied Energy, 254, 113660.
- 431 Roni, M. S., Thompson, D., Hartley, D., Searcy, E., & Nguyen, Q. (2018). Optimal blending management of
- 432 biomass resources used for biochemical conversion. *Biofuels, Bioproducts and Biorefining*, *12*(4), 624-648.
- 433 Shi J, Thompson V, Yancey N, Stavila V, Simmons BA, Singh S. Impact of mixed feedstocks and feedstock
- 434 densification on ionic liquid pretreatment efficiency. Biofuels. 2013;4(1):63-72.
- Shinners K, Bennett R and Hoffman D, Single-and two-pass corn grain and stover harvesting. Trans ASABE
 55(2):341–350 (2012).
- 437 US DOE (2020). Department of Energy (2020, March 23).
- 438 US Energy Information Administration (2019). U.S. Fuel Ethanol Plant Production Capacity. (2019, January 1).
- 439 US EPA (2020). Environmental Protection Agency. Overview for renewable fuel standard (2020, March 23).
- 440 Zhu, X., & Yao, Q. (2011). Logistics system design for biomass-to-bioenergy industry with multiple types of
- 441 feedstocks. *Bioresource technology*, *102*(23), 10936-10945.

1	ASABE Author Information
2	
3	THE NTH-PLANT SCENARIO FOR BLENDED FEEDSTOCK
4	CONVERSION AND PREPROCESSING NATIONWIDE: BIOREFINERIES
5	AND DEPOTS
6	T. Hossain, D. Jones, D. Hartley, M. Griffel, Y. Lin, P. Burli, D. N. Thompson, M. Langholtz, M.
7	Davis, C. Brandt
8	The authors are Tasmin Hossain, Graduate Research Assistant, Daniela Jones, Research Assistant
9	Professor, Department of Biological and Agricultural Engineering, North Carolina State University,
10	Raleigh, NC, USA, Damon Hartley, Group Lead of Biomass Analysis Group, Mike Griffel, Data
11	Scientist, Yingqian Lin, Research Scientist, Pralhad Burli, Economist, David N. Thompson,
12	Distinguished Staff Engineer, Idaho National Laboratory, Idaho Falls, ID, USA, and Matthew Langholtz,
13	Natural Resource & Environmental Economist, Maggie Davis, Natural Resource Data Scientist, Craig
14	Brandt, Statistician, Oak Ridge National Laboratory, Oak Ridge, TN, USA. Corresponding author:
15	Tasmin Hossain, Department of Biological and Agricultural Engineering, North Carolina State University,
16	3100 Faucette Drive, Campus Box 7625, Raleigh, NC 27695; phone: 984-202-9363; email:
17	thossai@ncsu.edu.

			Is the start date after
	ASABE		1 January 2016?
Funder	use only	Grant or award number(s)	yes/no/don't know
USDA	10.13039/100000199	Hatch Project Funds	Yes
NSF	10.13039/100000001		
USGS	10.13039/100000203		
USDOE	10.13039/100000015	DE-AC07-05ID14517	Yes